# Plasma-catalytic Selective Reduction of NO with C<sub>2</sub>H<sub>4</sub> in the Presence of Excess Oxygen

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**Abstract:** This paper reports observations of significant synergistic effects between dielectric barrier discharge (DBD) plasmas and Cu-ZSM-5 catalysts for  $C_2H_4$  selective reduction of NO<sub>x</sub> at 250 °C in the presence of excess oxygen by using a one-stage plasma-over-catalyst (POC) reactor. With the reactant gas mixture of 530 ppm NO, 650 ppm  $C_2H_4$ , 5.8%  $O_2$  in N<sub>2</sub> and GHSV = 12000 h<sup>-1</sup>, the pure catalytic, pure plasma-induced (discharges over fused silica pellets) and plasma-catalytic (in the POC reactor) NO<sub>x</sub> conversion are 39%, 1.5% and 79%, respectively. The *in-situ* optical emission spectra of the reactive systems imply some short-lived active species formed from plasma-induced and plasma-catalytic processes may be responsible to the observed synergistic effects in this one-stage POC system.

Keyword:  $NO_x$  removal, selective catalytic reduction, non-thermal plasma, CuZSM-5, ethene, optical emission spectroscopy.

The selective catalytic reduction (SCR) of  $NO_x$  using the addition of reductants such as NH<sub>3</sub>, urea, hydrocarbons, alcohols, has been studied intensively as a potential method to remove NO<sub>x</sub> from exhaust gases with excess  $oxygen^{1,2}$ . For availability reasons, the use of hydrocarbons as reducing agent (HC-SCR) has been of special interest in last 15 years. But the effective temperature window of those catalysts is relatively narrow, and should be broadened to lower temperatures for practical applications. One of the attempts to improve the catalyst property, especially at low temperatures, is of using non-thermal plasma and combined catalyst systems<sup>3,4</sup>. Under certain conditions, a better performance can be achieved by a catalytic post-treatment of the non-thermal plasmas effluent in the two-stage plasma-followed-by-catalyst (PFC) hybrid system<sup>3</sup>. However, for many cases, this solution is not very effective. Roland *et al.*<sup>5</sup> considered that real synergy effects between non-thermal-plasmas and catalysis can be expected by introducing the catalyst into the discharge zone, *i.e.* the one-stage plasma-over-catalyst (POC) system. To our knowledge, there are very few examples of reporting synergistic effects between plasma and catalysts in one-stage POC systems in literatures. Very recently, our laboratory<sup>6</sup> has pointed out that significant amounts of NO<sub>x</sub> can be generated

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from N<sub>2</sub> and O<sub>2</sub> in a one-stage POC reactor at temperatures higher than 300°C very likely *via* reactions between the plasma-produced N atoms and the catalyst-activated O<sub>2</sub> molecules. This article reports observations of an unambiguous synergistic effect between DBD plasmas and Cu-ZSM-5 catalysts in a one-stage POC reactor for C<sub>2</sub>H<sub>4</sub>-selective-reduction of NO<sub>x</sub> in the presence of excess oxygen around 250 °C.

### Experimental

The one-stage POC reactor used in this work consists of a fused silica tube (id 10 mm), a stainless steel tube (od 2 mm) placed along the axis of the outer tube as the high-voltage electrode and 2 mL of catalyst pellets (20-40 mesh) filled between the two tubes. A stainless steel wire mesh wound on the outside surface of the outer tube was used as the ground electrode. The DBD power supply source is capable of supplying a bipolar sine wave output with 0-40 kV peak-to-peak voltage,  $U_p$ , at an a.c. frequency of 50 Hz. The input electric discharge power at a certain experimental condition was measured via the area of the voltage-charge Lissajous figures<sup>8</sup>. The input discharge energy density in JL<sup>-1</sup>,  $E_{in}$ , can be controlled by adjusting  $U_p$ . An electric oven was used to heat the plasma-catalytic reactor. The gas flow makes the outside temperature  $T_{out}$  higher than the central one  $T_c$  without discharges. When the discharge is applied,  $T_c$  increases somehow. The average of  $T_c$  and  $T_{out}$  was taken as the reaction temperature,  $T_{reac}$ . The Cu-ZSM-5 catalysts were prepared via a ion exchange method, which was described previously<sup>9</sup>. The individual NO and NO<sub>2</sub> concentrations were monitored by a chemiluminescence analyzer (Monitor, ML9841AS). The concentrations of  $N_2O$  in the outflow gas were determined by an infrared absorption spectrometer (SICK- MAIHAK -S710). The optical emission spectra (200-900 nm) from the center of the catalyst bed of the one-stage POC reactor during discharges were measured by a monochromator (Acton-SP-300i). A quartz focal lens, placed near a quartz window on the wall of the heated oven, was used to collect the emission light into the entrance slit of the monochromator through an optical fiber.

### **Results and Discussion**

**Figure 1** shows the NO<sub>x</sub> conversion over Cu(165)-ZSM-5 and fused silica pellets in the one-stage POC reactor at  $T_{reac} = 250$  °C as a function of input discharge energy density,  $E_{in}$ . Under this temperature, the pure NO<sub>x</sub> SCR activity over fused silica pellets ( $E_{in} = 0$ ) are low (<1%) and the plasma-induced enhancements over fused silica are also small for the whole input discharge energy density range investigated (78-283 JL<sup>-1</sup>). In contrast to this, over Cu(165)-ZSM-5, the significant plasma-enhanced effects for C<sub>2</sub>H<sub>4</sub>-SCR of NO<sub>x</sub> have been observed and the rising  $E_{in}$  from 78 to 283 JL<sup>-1</sup> causes a monotonic increase of the NO<sub>x</sub> conversion. The slight decrease of NO<sub>x</sub> conversion after  $E_{in} > 155$  JL<sup>-1</sup> may reflect that an optimum electron energy range is probably needed for the plasma-assisted NO<sub>x</sub> catalytic conversion.

At  $E_{in} = 155 \text{ JL}^{-1}$ , the DBD plasma generates a maximal enhancement for the NO<sub>x</sub> conversion over Cu(165)-ZSM5. The NO<sub>x</sub> SCR conversion over Cu(165)-ZSM-5 With-

**Figure 1** NO<sub>x</sub> conversion over Cu(165)ZSM-5 or fused silica pellets in the one-stage POC reactor with or without discharge as a function of input discharge energy density.



Reaction conditions: 250°C, 530 ppm NO, 650 ppm C<sub>2</sub>H<sub>4</sub>, 5.8% O<sub>2</sub> in N<sub>2</sub>

out discharges ( $E_{in} = 0$ ), 39%, and over fused silica pellets with discharges,1.5%, were taken as the "pure catalytic" and "pure plasma-induced" conversion, respectively. The corresponding plasma-catalytic NO<sub>x</sub> conversion over Cu(165)-ZSM5 in the one-stage POC reactor,79%, reflects an unambiguous synergistic effect between the plasma and the catalyst. At the experimental conditions, the N<sub>2</sub>O content in the outflow gas of the POC reactor was less 8 ppm. And the input electric discharge power was determined *via* the area of voltage-charge Lissajous figures to be 0.94 W, which corresponds to an energy assumption of 84 eV per converted NO molecule.

Below  $T_{reac} = 200^{\circ}$ C the pure (without discharges) catalytic activity of Cu(165)-ZSM5 for C<sub>2</sub>H<sub>4</sub>-SCR of NO<sub>x</sub> is very low and the enhancement from the DBD plasma is also insignificant. At  $T_{reac} = 300^{\circ}$ C, the pure SCR activity reaches a maximum and the plasma exhibits a negative effect to the NO<sub>x</sub> conversion. As we pointed out previously, this is very likely related to the plasma-catalytic production of NO<sub>x</sub> from N<sub>2</sub> and O<sub>2</sub> at higher temperatures<sup>6</sup>.

The plasma-enhanced  $C_2H_4$ -SCR of NO over Cu(165)-ZSM5 in the one-stage POC reactor as a function of  $O_2$  concentration has been investigated at  $T_{reac} = 250 \text{ °C}$  and  $E_{in} = 155 \text{ JL}^{-1}$ . Similar to all the pure HC-SCR of NO cases, addition of certain amount of oxygen, promoting the oxidation of NO to NO<sub>2</sub>, or hydrocarbons to some oxidative derivatives, may play positive roles for NO<sub>x</sub> reduction. When  $O_2$  concentration is higher than 10%, the NO<sub>x</sub> conversion is decreased probably due to the increased prohibition of oxygen to the adsorption of NO<sub>x</sub> and  $C_2H_4$  on the catalyst.

To determine gas phase active species in the one-stage POC system, *in-situ* optical emission spectra (200-900 nm) have been investigated under  $E_{in} = 155 \text{ JL}^{-1}$  over fused silica and Cu-ZSM-5 pellets at 250°C with gas mixtures: (a) 530 ppm NO in N<sub>2</sub>, (b) 650ppm C<sub>2</sub>H<sub>4</sub> in N<sub>2</sub> (**Figure 2 a,b**). In both of cases, stronger emissions from discharge over fused silica pellets were observed than that from over CuZSM-5, very likely because of the higher optical reflectivity of fused silica and its much lower surface area, the excited species may be quenched through their collisions with the solid surface.

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**Figure 2** *In-situ* optical emission spectra under  $E_{in.}$ = 155 JL<sup>-1</sup> at 250 °C over Cu(165)ZSM-5 and fused silica pellets with different reacting gas mixtures: (a) 530 ppm NO in N<sub>2</sub>, (b) 650 ppm C<sub>2</sub>H<sub>4</sub> in N<sub>2</sub>



The observations of N<sub>2</sub> second positive band  $(C^3\Pi \rightarrow B^3\Sigma)$ , NO $\gamma$ -band  $(A^2\Sigma \rightarrow X^2\Pi)$ and a C<sub>2</sub>H<sub>4</sub>-related band with different gas mixtures imply that some short-lived active species formed from plasma-induced or plasma-over-catalyst-induced processes, such as C<sub>2</sub>H<sub>4</sub> fragments, partially oxidized hydrocarbons, electronically excited NO<sub>x</sub> species in the gas phase or vibrationally excited NO<sub>x</sub> species on the catalyst surface may be partially responsible to the observed synergistic effects between plasmas and catalysts in the one-stage POC system. Since O<sub>2</sub> molecule is a very efficient quencher for some electronically excited species, NO  $\gamma$ -band and the small C<sub>2</sub>H<sub>4</sub>-related peak disappeared when 5.8% O<sub>2</sub> was added into the gas mixture.

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